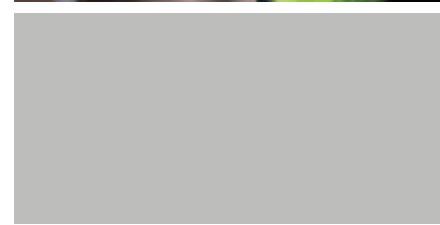


VA



U.S. Department
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Facilities Management



Steam, Heating Hot Water, and Outside Distribution Systems design manual

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Volume 1

STEAM BOILERS

(Steam Generating Systems)



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Table of Contents

1.0	DESIGN PARAMETERS/REQUIREMENTS	3
2.0	GENERAL CRITERIA.....	4
3.0	HEATING PLANT	6
4.0	EQUIPMENT LAYOUT	11
5.0	BOILER ROOM ENVIRONMENT	12
6.0	SYSTEMS AND EQUIPMENT	12
7.0	FUEL	17
8.0	BURNERS	19
9.0	COMBUSTION AIR	19
10.0	BOILER STACK AND EMISSIONS	22
11.0	CONTROLS AND INSTRUMENTATION	22
12.0	OPERATION OF BOILERS	24
13.0	FREEZE PROTECTION.....	25
14.0	WARRANTY	25
15.0	MODIFICATIONS TO EXISTING PLAN.....	25
16.0	CODES & STANDARDS	25
17.0	REFERENCES.....	25



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1.0 DESIGN PARAMETERS/REQUIREMENTS

1.1 Requirements:

- 1.1.1 This volume of the design manual establishes VA requirements on the quantity, capacity, arrangement, and standby capability of the boilers and auxiliary equipment. It applies to the design of new boiler, boiler replacement, and modification of existing boiler(s), in all climates.
- 1.1.2 The requirements of this manual shall apply to all steam boilers whether they are centralized systems or decentralized systems.
- 1.1.3 Decentralized systems shall comply to all the equipment requirements defined herein however the following elements will only be required for mission critical, hospitals, CLCs and inpatient facilities
 - 1.1.3.1 The system shall be capable of supplying the maximum steam demand with the largest boiler not operating, and with the largest pump of each service not operating (N+1 capacity)
 - 1.1.3.2 Dual Fuel capability with appropriate reserve capacity
 - 1.1.3.3 Emergency generator power requirements
- 1.1.4 Steam boilers and associated equipment whether central or decentralized shall be located in a secure, conditioned, and protected building and shall provide the appropriate security and weather protection in all climates. Additionally the building/room shall be equipped with combustible gas and CO monitoring that is alarmed locally as well as reports to a central location that is continuously monitored.

1.2 Load Determination Capacity Calculations:

- 1.2.1 Maximum loads shall be determined by adding existing demand, new connected loads and an allowance for future expansion required for planned projects. Boiler auxiliary equipment loads and distribution line losses shall be included in load calculations. Existing loads should be determined by installing a calibrated flow meter that will log real time data at a minimum of 5 minute intervals and totalize daily during the winter periods when the outside temperature approaches ASHRAE design conditions, and for summer periods in order to determine minimum flow. The accuracy of the data must be verified through review of meter calibration data and measurement logging criteria (i.e. hourly, hourly average or peak hourly). In the review of the data, judgment must be utilized in determining realistic peak loads (loads which are sustained for at least ten minutes).
- 1.2.2 Heat recovery and/or combined heat and power boilers shall not be included in the boiler plant capacity calculation unless they can operate with their own burners independent of the device from which heat is being recovered.

1.3 Boiler System Capacity:

- 1.3.1 The boiler system shall be capable of supplying the minimum demand with the smallest boiler in a normal mode of operation and with all auxiliary equipment operating within recommended turn-down ranges. The capacity of the smallest boiler shall be sufficient for peak demand in the non-heating season.



- 1.3.2 The boiler system shall be capable of supplying the maximum demand with the largest boiler not operating, and with the largest pump of each service not operating.
- 1.4 Boiler header pressure:
 - 1.4.1 Boiler Header pressure shall be sufficient to serve the pressure requirements of the loads in an economical manner.
 - 1.4.2 When replacing an existing boiler, header pressures shall not be changed (raised or lowered) from the existing unless a complete engineering analysis is performed on affected portions of the steam system of the facility to determine the effect of higher/lower pressures and temperatures on pipe expansion devices, steam traps, control/safety valves, equipment and other devices. Additionally the system shall be pressure tested at 1.5 times the updated pressure to ensure all components are capable of operating at the revised pressure. The performance of equipment supplied by the steam shall also be verified through commissioning and performance testing.
- 1.5 Boiler Plant Heat Recovery
 - 1.5.1 Provide heat recovery devices when they can be justified by a life cycle cost analysis. Systems may include
 - (1) Flue gas economizers for each boiler and
 - (2) Continuous blowoff heat recovery and
 - (3) Co-generation

2.0 GENERAL CRITERIA

- 2.1 Graphic Standards:
 - 2.1.1 Central plant heating, high pressure, low pressure boilers, and decentralized boilers work shall only be indicated on "MP"- series drawings (see *VA Design and Construction Procedure, Topic 2, Drawings*).
 - 2.1.2 "MP"- series drawings shall include symbols and schedules, equipment lists, schematic piping diagrams, floor plans, upper level plan of boiler room, mezzanine and pit plans, sections, demolition plans, fuel tank plot plans, and other work as necessary.
 - 2.1.3 Drawings must show plan and elevation views of all valves and equipment which require access and have both North and True North annotated.
 - 2.1.4 Flow sheets with instruments and flow/capacity shall be included in the design package. Instruments and equipment shall have unique tag numbers that are correlated to an instrument and equipment index. Tag numbers shall be coordinated with the shops to ensure standard nomenclature is aligned with local facility.
 - 2.1.5 Water treatment systems are shown on "PL" drawings.
 - 2.1.6 Fuel Gas piping shall be shown on the MP drawings.
 - 2.1.7 Structural drawings must show sufficient structural detail for each hanger and support location.
 - 2.1.8 Pipe size and material of construction shall be indicated for all piping, including those referring to existing conditions.
 - 2.1.9 Existing work which remains in service shall be identified in a way which easily distinguishes it from the new work.
 - 2.1.10 The standard symbol for point of connection, new work to existing shall be used. A similar symbol with the circle entirely filled-in shall be used to indicate extent of



demolition.

- 2.1.11 Dashed lines shall be used to distinguish material to be demolished.
- 2.1.12 Equipment shall be listed and scheduled in conformance with VA National CAD Standard details: <http://www.cfm.va.gov/til/sDetail.asp#23>
- 2.1.13 Show work on drawings using a minimum scale of 1:50 (1/4" = 1'0").
- 2.1.14 Steam and water piping and equipment arrangement must conform to the VA National CAD Standard.

2.2 Guidelines:

- 2.2.1 Heating systems requirements shall follow the HVAC Design Manual for New, Replacement, Addition and Renovation of Existing VA Facilities.
- 2.2.2 Design all equipment and systems to comply with this design manual, and the current editions of VA Program Guides, VA Handbooks and VA Master Specifications. The design shall also meet the provisions of all codes and regulations having jurisdiction and referenced in this document.
- 2.2.3 The latest edition of the VHA boiler plant safety device testing manual to ensure the appropriate arrangement and equipment are provided on the boiler and associate systems to accommodate the required testing.
- 2.2.4 If state or local codes are more stringent than the above requirements request clarification from the VHA authority having jurisdiction.
- 2.2.5 Earthquake-resistive design shall comply with the requirements of Master Specification Section 13 05 41, Seismic Restraint Requirements for Nonstructural Components, and the latest edition of the H-18-8 Seismic Design Handbook.
- 2.2.6 The facility/boiler system shall comply with the latest edition of the VA Physical Security Design Manual (PSDM).

2.3 Equipment selection

Equipment selection shall be non-proprietary. When as a standard of quality, model numbers are specified, the "Basis of design" designation must be added. When specifying by model number "Basis of design", the salient characteristics of the specified item which equality would be judged must also be included.

2.4 Life Cycle cost analysis

- 2.4.1 The DOE requires that agencies must estimate the life-cycle costs and energy consumption of a building and compare it to the minimum criteria set forth in the applicable baseline ASHRAE or IECC standard. This measure is meant to demonstrate and record the extent to which the mandated compliance is achieved.
- 2.4.2 Life Cycle analysis shall include at least three unique options for the solution of the project.
- 2.4.3 An engineering and economic analysis shall be performed in accordance with the procedure outlined by the DOE in the latest edition of the National Institute of Standards and Technology (NIST) Handbook 135 -Life –Cycle Costing Manual for the Federal Energy Management Program. The DOE 2 program shall be utilized when performing the required BLCC analysis using the following parameters:



2.4.3.1 Life-Cycle period:

<u>Equipment</u>	<u>Useful Life Expectancy (in years)</u>
i) Fire tube boilers and burners	30
ii) Water tube boilers and burners	40
iii) Feed water Deaerator	30
iv) Economizers	15
v) Burner management controls	20
vi) Combustion controls	20
vii) Instrumentation	20
viii) Boiler feed and condensate pumps	20
ix) Condensate and blow-off tanks and heat recovery	40
x) Fuel oil pumps	40
xi) Fuel oil tanks	40
xii) Valves, shut off and control	20
xiii) Water treatment equipment	20

2.4.3.2 Discount factor as determined by DOE on Oct 1st of each year.

2.4.3.3 Include initial acquisition costs such as:

- planning, design, purchase
- construction and capital replacement costs
- operating costs, such as energy used, water used,
- operating, maintenance, and repair costs
- Taxes and insurance need not be included in the life-cycle cost analysis.

2.4.3.4 Analysis of options shall be based on the system maintained and operating as designed. If the existing system is found to be deficient in one of these areas the analysis shall estimate the cost of correction and use that as the basis of the analysis.

2.4.4 Investigate the possibility of purchasing steam from a neighboring facility if purchasing steam is feasible. An evaluation should be made as to how often service from this facility has been disrupted. Additionally the need for an agreement for the supply of steam must be analyzed and included in the cost analysis addressing such items as the following:

- Rates and ability to ensure stable and agreed on escalation
- The resilience of the plant related to backup fuel and electrical
- The maintenance and upgrade program for the supplier
- The priority of the VA during load shedding.

2.4.5 Perform a life cycle cost analysis of purchased steam versus VA-generated steam including all expense factors such as boiler plant investment, fuel cost, salaries of operating personnel, maintenance costs, and electricity and water costs.

3.0 HEATING PLANT

3.1 General:



- 3.1.1 Heating plants can be either centralized or decentralized. The determination of what style plant a facility should install or whether a conversion is appropriate requires a detailed evaluation of many elements including installation, operation and maintenance. All new or converted plants shall analyze the following in a detailed engineering report prior to progressing to schematic engineering. The report shall be submitted to the Office of Capital Assets Management, Engineering and Support for review and comment.
- 3.1.2 Net present value of each option. The analysis should consider
 - 3.1.2.1 Capital cost
 - 3.1.2.2 Cost of replacement equipment during operational period
 - 3.1.2.3 Operational cost
 - 3.1.2.4 Energy as discussed in the latest edition of VA sustainable Design & Energy Reduction Manual and VA Directive 0055.
 - 3.1.2.5 Maintenance cost
 - 3.1.2.6 Resilience and cost impact of vulnerable areas (such as cost of vacating a building due to loss of heating equipment or cost of repairs due to loss of heating equipment)
- 3.1.3 The building and site adjacent to the building shall be arranged to allow for future expansion of additional boilers, chillers, or other equipment are needed.
- 3.1.4 Locate the heating plant in a separate building or room constructed per all applicable codes.
- 3.1.5 Any co-generation equipment should also be included in this building. The heating plant and the air conditioning chiller plant may be combined into an energy center building/central utility plant. For chiller plant requirements, refer to HVAC Design Manual.
- 3.2 Building Requirements
 - 3.2.1 Pipe, Breeching and Stack Supports and Anchors
 - 3.2.1.1 Provide a structural system which permits access to overhead members for pipe and duct support and allows for future expansion.
 - 3.2.1.2 Detail the design and locations of all roller and spring-type hangers, anchors, trapezes, seismic bracing and special supports. Detail the anchor designs and seismic bracing designs. Detail the connections to the building structure when standard pipe hanger components cannot be used as building attachments.
 - 3.2.1.3 Specific support, anchor and hanger information/data shall be provided on the design drawings by the engineer of record that created the drawings including but not limited to the following:
 - 3.2.1.3.1 Types, sizes, locations, and spacing of all hangers and supports.
 - 3.2.1.3.2 Roller or slider supports for all horizontal steam and condensate piping.
 - 3.2.1.3.3 Special supports including anchors, guides and braces.
 - 3.2.1.3.4 Supports to permit removal of valves and strainers from pipelines without disturbing supports.
 - 3.2.1.3.5 Spring hangers on all systems subject to vertical movement.
 - 3.2.1.3.6 Roller hangers and sliding supports on all systems subject to



- horizontal movement.
- 3.2.1.3.7 Loads for all supports. On systems utilizing variable spring supports, show the loads at each support by calculating the forces and moments throughout the system. Seismic restraint calculations shall utilize the applicable shock spectra for the type of structure, type of supported system, and the locality.
- 3.2.1.3.8 Individual detail for each hanger, anchor and support assembly showing all components, sizes, and calculated loadings. Provide identification tags on each keyed to the layout drawings.
- 3.2.1.4 Design steam systems for boiler plant header pressure and temperature (150 psig, 370 degrees °F) minimum, and design condensate systems for (100 psig, 200 degrees °F). Pipe stresses must not exceed allowable stresses calculated in accordance with ASME B31.1, ASME Code for Pressure Piping, Power Piping.
- 3.2.1.5 Vertical deflection shall not exceed 2.5 mm (0.1 inch) between supports when system is filled with fluid normally carried. Deflections due to seismic shock shall be restrained as necessary to prevent overstressing the supported system or the connected equipment. Seismic restraints shall permit movement due to thermal expansion.
- 3.2.1.6 If vertical angle of hanger rod exceeds four degrees, rollers or sliders are required.
- 3.2.1.7 Provide analysis of system stress and required expansion considerations and support/anchor requirements performed and stamped by a registered professional engineer.
- 3.2.1.8 Seismic Bracing for systems that experience thermal expansion shall be designed to allow the thermal expansion without overstressing any components.
- 3.2.2 The building design shall permit all equipment to be installed (and removed in the future) without removal of any building structural element, walls or the roof. (The exception being a designed knockout panel). This shall be clearly described and indicated on the design documents.
- 3.2.3 Locate the main boiler room floor above finished grade and the flood plain per PSDM to permit horizontal rigging of equipment in and out of the building.
- 3.2.4 Establish roof height to provide adequate clearance above all equipment and piping, for maintenance and operation. Clearance shall be a minimum of 15 feet from the top of the boilers and ancillary equipment to the roof line or the ceiling. Provide for present or future installation of economizers above the boilers.
- 3.2.5 Condensate storage tank, condensate transfer pumps, and fuel oil pumps should be designed to eliminate the need to be in a basement as these pieces of equipment are critical to the resilience of the plant. Installation of this equipment in pits is prohibited. If a basement is required, additional water proofing and flood protection shall be provided in the form of duplex pumping systems with redundant backup and powered with emergency power. Duplex sump pumps should be submersible to mitigate issues with potential failure due to motor flooding. .
- 3.2.6 Locate a mezzanine above the boiler feed pump area to support and provide access to the deaerating feedwater heater. Normal mezzanine floor height above the boiler room floor is 12 feet. Design the mezzanine floor to contain/eliminate water spillage/leakage



- without damaging equipment below.
- 3.2.7 Provide overhead roll-up doors through which all equipment can be rigged. Locate a roll-up security grill inside each door so that the doors can be open for summer ventilation.
 - 3.2.8 Boiler room shall be designed with double access (2-doors).
 - 3.2.9 Combined Boiler and Chiller Plants (Energy Centers/Central Utility Plant)
 - 3.2.9.1 Combining the boiler and chiller plant in one building is preferred when it can be economically justified. Each proposed energy center must be reviewed by VA Central Office.
 - 3.2.9.2 The energy center shall house the boiler plant, chiller plant, Engineering Control Center, pumps, plumbing equipment, associated electrical switchgear and boiler plant emergency generator and co-generation equipment for the VA medical center. To the extent feasible other emergency generators and electrical substations and domestic hot water generators may be placed in the energy center.
 - 3.2.9.3 The chiller area and the Engineering Control Center shall be designed in accordance with the HVAC Design Manual.
 - 3.2.9.4 The electrical equipment area shall be designed in accordance with Design and Construction Procedure, and VA Design Manual for Engine-Generators and Distribution.
 - 3.2.10 The building design shall be such that the Safety Relief Valve Vent piping will exit the roof directly above the equipment for which it serves. The maximum degree of directional change after the drip ell is limited to 180 degrees. All directional changes shall be done with 45's or long radius sweeping 90's.
 - 3.2.11 Trench type drains shall be designed and installed on both sides of the boilers and other equipment. The DA tank and Condensate tank overflow shall go to a drain rated for the temperature of the DA tank when in normal operation.
- 3.3 Water Treatment Area (central or hub locations):
- 3.3.1 Provide an area which includes the chemical feed units and space for chemical storage and mixing. Cold water and drains must be available in the area and there must be an emergency eyewash and shower. Approximate floor space requirement for chemical storage is 100 square feet. The chemical storage area must accommodate chemicals in barrels or bulk tanks that will be furnished by the chemical supplier. The storage area must be reachable by hose from a tank truck parked outside the building. If dry chemical is used there must be access from the outside for fork truck or hand truck transport and platforms for loading into system.
- 3.4 Water Test Area (central or hub locations):
- 3.4.1 Provide laboratory type sinks in a stainless steel countertop unit which includes cabinets below and above for storage of boiler water testing equipment. Locate boiler water sample coolers adjacent to the sink unit. The test area should be adjacent to the firing aisle. The feed water sample cooler should be located adjacent to the deaerator.
- 3.5 Personnel Facilities
- 3.5.1 An air conditioned control room of at least 150 square feet floor area with view
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windows located to allow observation of boiler aisle and chillers. Where an Engineering Control Center is provided additional floor area is required (see Chapter 230 of VA Handbook 7610 for required floor area).

- 3.5.2 A supervisors' office of approximately 100 square feet floor area.
- 3.5.3 Locker facilities on the main floor of boiler plants and energy centers for employees, one or more of which will be female. Facilities shall include separate showers and locker rooms for male and female employees. Twelve lockers shall be provided including a minimum of two lockers in the female locker area.
- 3.5.4 Two separate toilet rooms adjacent to the locker rooms each having a water closet and lavatory plus a urinal in male toilet.
- 3.5.5 Water cooler.
- 3.5.6 Break room with sink, storage cabinets, and electric service for microwave oven and refrigerator.
- 3.5.7 Housekeeping closet.
- 3.6 Access Platforms
 - 3.6.1 Provide a platform above each boiler to provide access to valves and manways which are located on top of the boiler. Minimum width shall be 2.5 feet, with length to suit boilers furnished.
 - 3.6.2 A three feet x four feet steam drum manway access platform at the rear of each water tube boiler. Locate below the steam drum.
 - 3.6.3 Provide platform for access to economizer valves and service panels.
 - 3.6.4 Provide other platforms as necessary to allow access to equipment requiring maintenance.
- 3.7 Permanent ladders and stairs
 - 3.7.1 Provide stairways to mezzanine, platform or pit levels which require frequent access, such as deaerator level.
 - 3.7.2 Provide permanent ladders for access to all platforms. The design of ladders and platforms shall conform to OSHA requirements.
- 3.8 Acoustical Considerations
 - 3.8.1 Provide acoustical treatment on building surfaces which are within three meters (10 feet) of burner fans or atomizing air compressors or co-generation engines. Provide noise control in the operations room/Engineering Control Center and in the office in accordance with VA Design and Construction Procedure, Noise Transmission Control.
 - 3.8.2 Provide a block wall partition between the chiller portion of the building and other areas for noise control. Also provide the same for the co-generation engine unless other noise reduction measures are taken.
- 3.9 Boiler Plant Building Hazardous Gas Detection System:
 - 3.9.1 Industrial-type system with central alarm panel and multiple sensors is required. Provide carbon monoxide sensors at breathing level near the front of each boiler and in personnel spaces where there is exhaust ventilation.
 - 3.9.2 If natural gas is a main fuel, provide combustible gas detectors at the ceiling of the boiler room. If propane is utilized as a main fuel, provide combustible gas sensors at the low points in the boiler plant.



- 3.9.3 Alarm shall be audio visual inside and outside the plant and labeled to identify the system it is protecting.

4.0 EQUIPMENT LAYOUT

- 4.1 In a central plant arrange boilers; co-generation equipment, emergency generator room, control panels, instrumentation panel, motor control center, and control room/Engineering Control Center shall be located along an aisle on the main floor. Boiler and chiller spaces must be observable from the control room/Engineering Control Center. Locate boiler feed pumps, water treatment area and main steam header on the main floor.
- 4.2 Control and instrument panels shall be visible from aisle, and to the maximum extent possible, visible from the control room/Engineering Control Center. Instrument panels may be located in the control room/Engineering Control Center.
- 4.3 The electrical switchgear and engine-generator(s) shall be located within the plant in a separate room adjacent to an outside wall. The engine-generator(s) shall be visible via view windows from the room that contains their paralleling and distribution equipment.
- 4.4 Heat Recovery Boilers: Heat recovery boilers generating high pressure steam shall be located in the boiler plant where they can be monitored by boiler plant operating personnel.
- 4.5 Housekeeping Pads - All floor mounted equipment shall be placed on and anchored to housekeeping pads
- 4.6 Tube replacement for firetube boilers generally requires a space in front of the boilers which is equal to its longest length. (See manufacturer's installation manuals for exact area required for boiler tube pulls.)
- 4.7 The width of the clear space between the side of a boiler and a wall shall be not less than 3 feet 6 inches.
- 4.8 Passage clearance between boilers ≥ 36 inches wide and ≥ 80 inches high.
- 4.9 The clearance for the opening of boiler doors shall be not less than 12 inches from the edges of the doors in any position.
- 4.10 The clearance between floor mounted pumps shall not be less than three feet. The clearance between floor mounted pumps and walls shall not be less than two feet, preferably three feet, except where a greater clearance is required to maintain a walking aisle.
- 4.11 Where possible allow enough space between boilers to maneuver a fork lift truck. Mandatory for new construction.
- 4.12 All equipment and piping devices must be accessible from the floor or from permanent platforms for operation, repair, maintenance and replacement.
- 4.13 Repair, maintenance and replacement must be possible without requiring the removal of other major items of equipment, the removal of major portions of piping, or the removal of portions of the building.
- 4.14 Generally, there should be at least three feet of clear floor space around all items of equipment. Boilers require a greater amount of clearance.
- 4.15 Control and instrument panels shall be visible from aisle, and to the maximum extent possible,



visible from the control room/Engineering Control Center. Instrument panels may be located in the control room/Engineering Control Center.

- 4.16 Where possible, valves shall be located not more than seven feet above a floor, mezzanine, or platform. Limited exceptions are permitted for valves that are rarely used, would not need to be operated in an emergency situation, and can be reached with portable ladders or chain-wheels.
- 4.17 Natural Gas compressors and piping for natural gas turbine cogeneration equipment shall be located outside of the boiler plant in a separate enclosure and comply with the requirements of Factory Mutual, NFPA, and industry standards where there is no specific VA guidance.
- 4.18 Access to boiler blow down valves is critical since steam boilers are to be blown down at least once every eight hours.

5.0 BOILER ROOM ENVIRONMENT

5.1 Heating Plant HVAC Requirements

- 5.1.1 Heating plant and energy center heating, ventilating, and air conditioning shall be provided as follows:
 - 5.1.1.1 Combustion and ventilation air intakes through the building walls and roof. Provide combustion air make-up heating and ventilating units in colder climates.
 - 5.1.1.2 The maximum plant temperature shall be limited to 104 degrees F (40 degrees C).
 - 5.1.1.3 Install roof-mounted exhaust fans to provide a minimum of 12 air changes per hour in the boiler areas (or more for to meet the maximum temperature defined).
 - 5.1.1.4 Heat occupied rooms (ECC, office, toilets, showers, break room) to maintain temperature, humidity, outside air, etc. according to the HVAC Design Manual.
 - 5.1.1.5 Heat (if necessary) the boiler room, chiller room and other equipment spaces to maintain 40 degrees F.
 - 5.1.1.6 Air conditioning shall be provided in the ECC, office, toilets, showers, break room only.
 - 5.1.1.7 Boiler room, chiller room shall be mechanically ventilated to maintain a maximum of 104 F. If either area is in excess 86 F spot coolers shall be provided at key operational areas and a portable for maintenance. Evaporative coolers such as "swamp coolers" are prohibited due to a potential of exposure to Legionella.

6.0 SYSTEMS AND EQUIPMENT

- 6.1 Definition of steam distribution pressure classes:
 - Low pressure steam (LPS).....0 thru 15 psig
 - Medium pressure steam (MPS).....Above 15 thru 60 psig
 - High pressure steam (HPS).....Above 60 psig
- 6.2 Boilers :
 - 6.2.1 Quantity of Boilers: Minimum three units are the most cost effective and operationally practical. In some cases, two large and a smaller boiler for use in the summer load



period is optimal. The selection should be based on the load profile developed by the design engineer and a life cycle cost analysis. Preferred method shall be to use separate smaller boiler for summer and larger boilers for winter.

6.2.2 Boiler Design:

Boiler steam output capacity shall be based on boiler heating surface requirements as follows:

6.2.2.1 Fire Tube Packaged Gas and/or Oil Boilers:

6.2.2.1.1 Packaged fire tube units up thru 6900 kW (700 boiler hp) are acceptable. Packaged water tube units are acceptable for any capacity requirement. The choice between water tube and fire tube units must be based on life cycle costs, and available space in the boiler room

6.2.2.1.2 Provide 0.019 square meter per kilowatt output (2 square feet per boiler horsepower).

6.2.2.2 Water Tube D- Type Packaged Gas and/or Oil Boilers:

Heating Surface (sq. meters) = (Output (Kg/Sec) x 60.6) + 60

Heating Surface (sq. ft.) = $\frac{\text{Output (BTU/Hr.)} + 700}{12,500}$

Heating surface is defined as the flat projected area in the furnace and full circumferential area in the convection section of the boiler. Furnace heat release shall not exceed 520,000 W/cu. meter (50,000 BTU/Hr. cu. ft.).

6.2.2.3 Other Types of Boilers:

Apply conservative ratings. Utilize other types, such as flex-tube boilers, only on non-critical loads.

6.2.3 Packaged Fire Tube Boilers

Packaged fire tube boilers may not be used for loads exceeding 23,400,000 BTU/hr. Packaged water tube units are acceptable for any capacity requirement.

6.2.4 Low load Operations

Watertube boilers shall not be required to cycle on and off. Cycling of firetube boilers must be kept to a minimum.

6.3 Pressure control and Relief

6.3.1 Provide dedicated steam pressure reducing valve (PRV) station(s) for each building and for each steam pressure station

6.3.2 Do not provide two-stage PRV station to reduce high-pressure steam pressure.

6.3.3 Provide two PRV's in parallel where significant variation in the steam demand is expected. For such applications, two PRV valves, of uneven sizes should be provided. The smaller valve (1/3 capacity) set at the desired control pressure shall open first and the larger valve (2/3 capacity) set at slightly below the small valve shall open next but only when the smaller valve is unable to meet the increasing load demand and resulting higher pressure drop.

6.3.4 Install a bypass loop with globe valve sized for the flow of the largest valve in the PRV station.

6.3.5 Size safety relief valve to handle the maximum flow of the largest PRV in the station, comply with National Board of boiler and pressure vessel inspectors and ASME code



requirements.

- 6.3.6 Provide isolation valves to accommodate maintenance of the PRVs while maintaining steam flow
- 6.3.7 Provide a pressure gage at the inlet and outlet of the station complete with isolation valve with a range and construction appropriate for the pressure.
- 6.3.8 Vent line from safety valve(s) at the PRV station shall be independent of other vent lines and shall extend a minimum of 6 feet above the roof.
- 6.3.9 For each steam PRV station provide a steam flow meter. Meter shall be connected to the Building automation system and be capable of logging instantaneous flow as well as totalized flow.
- 6.3.10 Shutoff Valve: For each incoming steam service, provide a shutoff valve and a 4.5 inch pressure gauge with a range appropriate for the pressure being read.

6.4 Condensate

- 6.4.1 To avoid flashing, the steam condensate gravity return system shall not contain connections between high pressure gravity returns or medium pressure gravity returns with the low pressure gravity or vacuum return lines. Provide a flash tank, where all gravity returns will reduce pressure and temperature. From the flash tank, the low pressure gravity return shall flow into the condensate receiver of the condensate return pump. Adjust the elevation of the flash tank elevation to ensure gravity flow into the condensate receiver.
- 6.4.2 Condensate Storage Tank shall be sized to accommodate surges without overflow. The tank shall be sized for 20 minutes minimum storage to overflow at peak plant output requirements. The A/E must review the condensate handling systems in all buildings to determine if any unusual situations will require a larger condensate storage tank in the boiler plant. Consideration should be given to sizing the tank for future loads.

6.5 Water Treatment Equipment

- 6.5.1 "Zero Hardness" water must be supplied for boiler makeup.
- 6.5.2 Water Treatment shall be provided if alkalinity in the makeup water exceeds 50 ppm. The design engineer must obtain a current analysis of the water supply and determine the type of treatment which is necessary. The design engineer must determine if the treated water will cause any substantial corrosion problems and recommend preventative methods.
- 6.5.3 Life cycle cost studies must be performed to evaluate which type of water treatment equipment will be applied (ion-exchange softener, dealkalizer, reverse osmosis, other systems) as proven successful with local water conditions.
- 6.5.4 Softeners shall be dual tower to ensure supply during regeneration. Bulk brine storage shall be used where possible to avoid material handling if not possible salt storage space adjacent to water softener and dealkalizer. The area should be accessible using fork truck for transport of bulk salt and a platform provided for loading the tanks.
- 6.5.5 Boiler Plant Chemical Feed Systems
 - 6.5.5.1 Provide a separate continuous feed system (proportioning pump and tank) for each boiler.
 - 6.5.5.2 System shall utilize premixed chemicals with multiple metering pumps for injection to eliminate the need for mixing and handling of the chemicals.



6.5.5.3 Provide sample coolers and sample points on feedwater, Hot water header supply and return and in the system as directed by the chemical treatment vendor.

6.6 Steam Traps:

Note: *Fixed orifice steam traps with no operating mechanism are prohibited due to the small diameter orifices that become plugged with dirt and cause the trap to fail shut. This will cause build-up of condensate in the steam main and dangerous water hammer may occur.*

- 6.6.1 Steam traps remove condensate and air from steam lines while at the same time preventing the loss of steam. A steam strainer shall be installed at the trap inlet to prevent scale or other solid particles from entering the trap.
- 6.6.2 Float and Thermostatic traps. Provide float and thermostatic (F & T) traps for all heating equipment having modulating loads such as heat exchangers, domestic hot water heaters, modulating control valves (where used) for preheat coils and equipment with modulating loads. Provide minimum 12 inches static head for the trap operation (18 inches where space permits). Size all F&T traps at 0.25 psig pressure drop. Capacity of a single trap shall not exceed 5,000 lbs./hr.
- 6.6.3 Inverted Bucket Trap. Steam traps on the steam line drip points shall be inverted bucket type, with bi-metallic thermal element for air removal. The trap pressure differential shall be 80% of the operating line pressure.
- 6.6.4 Drip traps shall be sized for the line radiation loss multiplied by 3 for start-up needs. (Condensate forms at a greater rate during warm up.)
- 6.6.5 Traps serving terminal heating equipment shall be sized for their steady state condensate load multiplied by 2.5 for startup needs.

6.7 Pumps

- 6.7.1 Provide one standby pump for each service except boiler feed systems where one pump is dedicated to each boiler. Pumps shall operate continuously rather than on-off. Motor kW (hp) shall be selected to be non-overloading at any point on the pump performance (head - capacity) curve with the largest available impeller. Variable frequency drives controlling discharge pressure may be applied on pumps equal to or greater than 7.5 hp.
- 6.7.2 Condensate Return Pumps
 - 6.7.2.1 Provide duplex condensate pumps, complete with a receiver, to return steam condensate to the boiler plant.
 - 6.7.2.2 Provide emergency power for the pumps and controls.
 - 6.7.2.3 The pumps shall be of a centrifugal type and shall generally be selected to operate at 1750 rpm.
- 6.7.3 Boiler Feed Pumps
 - 6.7.3.1 Arrangement shall be one pump dedicated to each boiler, with cross connections allowing each pump to provide emergency service to one other boiler. In the largest plants it may be advantageous to provide a boiler feed header system with all pumps supplying the common header.
 - 6.7.3.2 High efficiency multi-stage centrifugal pumps are preferred. Two-stage horizontal split case centrifugal pumps may be applied on larger plants if the life cycle cost is less than for multi-stage.



- 6.7.3.3 Provide emergency power to the pumps and controls
- 6.7.3.4 The pumps shall be of a centrifugal type and shall generally be selected to operate at 1750 rpm.
- 6.7.3.5 Allow space for a future pump.

6.8 Feedwater deaerators

- 6.8.1 Deaerators shall be provided to reduce corrosion. Due to enhanced turndown capabilities, tray and packed column types shall be used if there is sufficient building height available for the deaerating section which is mounted on the deaerated water storage tank. Where height is limited, spray-type units may be used.
- 6.8.2 The deaerated water storage tank shall be sized for 20 minutes storage from overflow level at peak plant output requirements. Consideration should be given to sizing the feedwater deaerator for future loads. Packaged boiler feed pump/deaerator units should not be applied except where there are space limitations.

6.9 Blowdown:

- 6.9.1 Blowdown is required to remove precipitated sediments and control the concentration of chemical additives by a valve. Continuous or intermittent manual blowdown may be used. Steam boilers shall be blown down at least once every eight hours.
- 6.9.2 Blowdown Tank:
 - 6.9.2.1 The tank shall be located within the boiler plant building or room.
 - 6.9.2.2 The blow-down tank inlet shall be at an elevation below the elevation of the blowdown header to prevent sludge from accumulating below the header. Where this is not possible provide water flushing system to clean trapped horizontal blowdown lines.
 - 6.9.2.3 Provide a drain with manual valve on the blowdown line to allow draining of the boilers.
 - 6.9.2.4 Blowdown tank size shall be in accordance with the recommendations contained in the Rules and Recommendations for the Design and Construction of Boiler Blowdown Systems published by the National Board of Boiler and Pressure Vessel Inspectors, Columbus Ohio.
 - 6.9.2.5 Blowdown tank volume shall be twice the volume of water contained in a four inch blowdown of the largest boiler.
 - 6.9.2.6 Provide an automatic temperature control system which uses either a blowdown recovery unit (preferred) or A blowdown cooler to limit the temperature of the water going to the sewer to 140 degrees F.

6.10 Emergency Power

- 6.10.1 A UPS must be provided to ensure that the control system is kept functional during power outages and transition.
- 6.10.2 Engine-Generators: Central plant shall be equipped with a dedicated generator/ATS located in appropriate room(s)/enclosure accessible by the operator without leaving the plant.
- 6.10.3 Any boiler that is decentralized shall be equipped with a dedicated automatic Transfer switch and powered by the facility electrical emergency service.
- 6.10.4 Generators, ATS and other components which comprise the Emergency Power Supply System (EPSS) shall be installed, operated, tested and maintained in accordance with



the latest edition of NFPA 110, Standard for Emergency and Standby Power Systems and with VHA Directive, Electrical Power Distribution System (latest version).

- 6.10.5 Sites with electric steam generators must have those generators connected to either the facility's essential electrical system (emergency power system) or a standby power system(s) dependent on the facility's risk analysis. On-site storage of generator fuel for boiler use must be sufficient for a minimum of 96 hours of continuous operation.

7.0 FUEL

7.1 General

- 7.1.1 Perform an engineering economic analysis to determine the lowest life cycle cost of various fuel options.
- 7.1.2 When considering fuel options, determine the reliability of the supply and the feasibility of using each fuel. Where natural gas is utilized, provide a second fuel (such as fuel oil or propane), stored on the site, as a standby.
- 7.1.3 Analysis of fuel must consider permitting and emission limit impacts on equipment.
- 7.1.4 Conform to local, federal and state emissions regulations.
- 7.1.5 Boiler fuel of choice is natural gas for reasons of supply security, equipment life and environmental compliance.
- 7.1.6 Propane shall be used for the operation of igniters (pilots) when natural gas is not available or has been interrupted. If natural gas is normally utilized, the LP gas igniter system is for emergency use only. The LP gas igniter system shall operate at 5 psig or less. The VAMC will supply replaceable propane cylinder tanks. The A/E must design the tank piping, valve system, and provide concrete pad and chains for supporting the tanks. Locate the tanks outside. Locate the tanks outside with setback as defined by code and protection as required by VA PSDM.
- 7.1.7 Standby Reserve Fuel storage quantity
 - 7.1.7.1 Facilities firing coal as fuel, shall store a sufficient supply of fuel to meet the normal demands of continuous operation for a period of 15 January days. If the facility is equipped with an on-site (stored) backup source of fuel such as natural gas, propane or fuel oil, the coal supply can be reduced to 10 days. The combination of on-site primary and backup fuel supply must be sufficient for 15 days of continuous operation in January. Plants that generate less than 50 percent of their annual steam demand by natural gas for two consecutive years are considered to be coal-fired, and shall meet the supply requirements for coal-fired plants.
 - 7.1.7.2 Facilities firing oil as fuel shall maintain a supply of fuel sufficient to meet the normal demands of continuous operation for a period of 15 January days. If the facility is equipped with a backup source of fuel such as natural gas, propane or coal, the oil supply can be reduced to 10 days. The combination of on-site primary and backup fuel supply must be sufficient for 15 days of continuous operation in January. Plants that generate less than 50 percent of their annual steam demand by natural gas for two consecutive years are considered to be oil-fired, and shall meet the supply requirements for oil-fired plants.
 - 7.1.7.3 Facilities firing natural gas as the main fuel with fuel oil or propane back-up shall



maintain a sufficient supply of back-up fuel to meet the normal demands of continuous operations for a period of 10 January days.

7.2 Natural Gas

- 7.2.1 Header pressure in the boiler plant shall be as low as practical which, for water tube boilers is 70 - 100 kPa (10 - 15 psig) and, for fire tube boilers is 35 - 70 kPa (5 - 10 psig). Higher gas pressures may be required for low-NO_x burners or high turndown burners. Coordinate system design with requirements of local gas supplier.
- 7.2.2 Provide separate gas meter for the boiler plant.
- 7.2.3 Provide emergency Gas shut off valve with emergency stop buttons at each exit from the plant or room. Protect buttons from accidental activation and provide signage to identify the purpose.

7.3 Fuel Tanks

- 7.3.1 May be located underground or aboveground. Provide secondary containment systems on tanks and piping. All steel buried tanks, piping, and secondary containment shall be coated and cathodically protected.
- 7.3.2 Provide electronic leak detectors located in the interstitial spaces of the tanks and in piping systems between the carrier pipes and outer casings. Provide spill and overflow prevention measures as required by pollution control authorities.
- 7.3.3 The use of day tanks is not preferred and should only be used when there is a situation that mandates such an arrangement.
- 7.3.4 Tanks shall have an automatic system for monitoring/measuring fuel level and alarming high and low levels. The system shall have both audible and visual indication and annunciation locally and at the operator station.
- 7.3.5 Tanks shall be equipped with recirculation filtering systems to ensure fuel quality.

7.4 Fuel pumps

- 7.4.1 Gear, lobe or screw style pump shall be used for boiler feed.
- 7.4.2 Fuel oil pumps shall be sized to accommodate the maximum flow based on the maximum design steam output with a 10% safety factor for future expansion or the known master plan expansion plan whichever is greater.
- 7.4.3 Fuel oil pumps shall be located above grade and protected from potential flooding due to weather or other action. There shall be a housekeeping pad for each pump or pump system.
- 7.4.4 Pumps arrangement shall be duplex with one operating and one standby.
- 7.4.5 Pump skid shall be equipped with a duplex strainer on the suction of the pumps and connections on the supply and discharge for emergency connection to the system.
- 7.4.6 Each pump will be equipped with a safety relief valve that relieves to the tank return complete with site glass to inspect for flow. The system shall have a backpressure control valve and associated pressure relief valves.
- 7.4.7 The system shall have a supply and return flow meter in the piping to the boilers system.
- 7.4.8 Refer to standard detail on the TIL for additional information.
- 7.4.9 Pumps shall be of a type suitable for the application and shall generally be selected to operate at 1750 rpm.



7.5 Fuel Oil piping

Oil piping shall be located in trenches to reduce hazard caused by leaks and air binding. Provide accessible drains in trenches for cleaning and removal of water from plant or rain. All drains serving chemical and petroleum systems shall be equipped with an oil/water separator (OWS). OWS shall be accessible for pumping by a vacuum truck.

8.0 BURNERS

8.1 Automated shutdown- When steam pressure is in excess of demand sensed, the following will occur:

- 8.1.1 The damper will return to low fire position
- 8.1.2 The operating limit control opens
- 8.1.3 The main fuel valve circuit is de-energized, main fuel valve closes.
- 8.1.4 Flame is extinguished
- 8.1.5 The running lights on the control panel turn off
- 8.1.6 The blower motor continues to force air through the boiler for the post purge period.

9.0 COMBUSTION AIR

9.1 An adequate air supply provides for clean, safe combustion and minimizes the formation of soot.

9.2 The boiler room shall have two combustion air openings to ensure adequate combustion air and proper ventilation; one within 12 inches of the ceiling and the other within 12 inches of the floor. Each opening shall have a minimum free area of 1 inch squared per 2000 BTU/hr. input rating (of all the burners in the plant). The designer shall ensure the plant is not negative with all boilers running at full load.

9.3 Combustion air fans shall be equipped with variable frequency drives.

9.4 Combustion dampers shall be interlocked with the boiler firing cycle. Manually operated dampers prohibited.

9.5 Burners:

Provide low excess air design, with oxygen trim, on larger water tube boilers when justified by life cycle cost analysis. Provide low NO_x burners (not to exceed 30 ppm) unless lower emission concentration is required by emissions authorities and local AHJ. Written confirmation of the AHJs requirements shall be obtained for the record.

- 9.5.1 Dual Fuel Burners: Dual burners are the required for VA Hospital applications. Burners shall be of the low pressure, air atomizing (nozzle) type. Burners feature ignition by spark-ignited gas pilot flame. With either fuel, the burner operates with full modulation. A switch permits changeover from automatic fully modulated firing to manually set firing at any desired rate between minimum and maximum. Additional safeguards assure that the burner always returns to minimum firing position for ignition. Dual burners are designed for automatic, unattended operation except for periodic inspection and maintenance. After selecting the proper overload settings for the starter, the rest of the control panel components require little attention except for occasional cleaning. Burner fuels to be used shall be based on availability and frequency



of service interruption.

9.5.1.1 The change from one fuel to another must contain hard wired switch interlocks to ensure the controls align with the fuel supply. Additionally the changeover shall not require changes to the fuel system piping or controls by the operator. Changeover shall also be accomplished without the need for special tools or hoisting equipment and should be able to be completed within 20 minutes by one operator.

9.5.1.2 Operating Controls: The burner is supplied with a remote control panel and with a burner mounted junction box.

9.5.1.3 The control panel contains a flame safeguard programming control, motor starters, relays, time delays and terminal strips mounted internally on a panel sub-base. Lights, switches, potentiometers, a control circuit breaker and flame safeguard displays are mounted externally on the panel. The burner control circuit operates on 115 volt, single phase, 60 hertz (or 50 hertz when required) alternating current. The flame safeguard and burner control shall be in separate cabinets to ensure complete separation and ease of troubleshooting. The wiring shall be independent and not passed through or dual use.

9.5.2 Gas Burners:

9.5.2.1 Gas train shall be in accordance with International Risk Insurance (IRI) Standards and shall meet the requirements of NFC 85 – Boiler and Combustion Systems Hazard Code – para 6. Single fuel burners are not recommended for Hospital applications.

9.5.2.2 The burners shall be the atmospheric type and constructed of stainless steel.

9.5.2.3 The firing mode shall be 4-stage control, which shall be electronically operated, and shall continually monitor the water temperature, staging the heater for the most efficient operation.

9.5.2.4 Maintain, service, inspect, and operate gas burners in accordance with the manufacturer's operation and service manual.

9.5.3 Oil Burners:

9.5.3.1 Oil burners must atomize and vaporize oil to get the oil into combustible form. Large burners usually prepare the oil for combustion by first atomizing the fuel and injecting it into the combustion space for final heating, vaporization and mixing with combustion air. Single fuel burners are not recommended for Hospital applications. Atomization is generally obtained by one of the following methods:

9.5.3.1.1 Horizontal Rotary Cup type:

In this method, a thin film of oil is spun from the rim of a cup being rotated at high speed. The oil enters a cone of high velocity primary combustion air where atomization is obtained. This type burner is capable of high maintenance costs and efficiencies.

9.5.3.1.2 Mechanical Pressure Atomizing type:

This method expands the oil by pressure through a small orifice thereby breaking it into a spray of very fine droplets. This burner is not adaptable to appreciable modulation as a drop in pressure



results in rapid deterioration in atomization efficiency. Mechanical atomization requires the highest oil pressure and yields the poorest performance.

9.5.3.1.3 Steam Atomizing type:

In this method, oil is delivered to the nozzle at pressures ranging from 40 to 150 psig with steam pressure not less than 20 – 50 psig. In most cases, steam atomizing can produce a turn-down of up to 10:1 at high efficiency. Steam for atomization must be dry as moisture causes erosion which impairs burner performance and causes pulsations which leads to loss of ignition. If steam is wet, oil cannot be properly atomized regardless of the amount of steam utilized. In general some superheat, possibly up to 50 degrees F, is desirable. The steam supply line should be of proper size, well insulated, and adequately drained. The first cost of a steam atomizing system is less, but it is about 1 percent less energy efficient than air atomization. The steam atomizing burner has a higher turndown rate than the air-atomizing types and is used whenever air atomization cannot obtain the same turndown ratio.

9.5.3.1.4 High-Pressure Air Atomizing type:

This method is similar to the steam-atomizing type except air under pressure is used instead of steam. High-pressure air atomizing burners utilize air pressures of 30 psig and above and can operate within the same range of oil pressures and preheat temperatures as the steam atomizing type.

9.5.3.1.5 Low Pressure Air-Atomizing type:

This system generally operates within ½ to five psig air pressure and five to 20 psig oil pressure.

9.5.3.1.6 Low-Excess Air type:

These burners are designed to operate with excess air down around 5 percent. These burners are high in first cost, and require excessive supervision and maintenance. Low excess air burners are used mainly to reduce nitrogen oxide (NOx) emissions. Only provide low NOx burners if required by the emissions authorities.

9.5.3.1.7 Low-NOx type:

Low-NOx burners have a wide variety of designs. The principle of all low-NOx burners is the same; they inherently generate lower NOx emissions due to internal staging of fuel combustion. The Low NOx burners are equipped with a Flue Gas Recirculation system (FGR). The flue gases are duct to the air housing and the burner combustion air fan is used to pull flue gases from the stack. The FGR rate is controlled by damper blade linked to the modulating motor. Top or bottom connection is used with a flanged adaptor to the damper box. Fresh air and FGR is mixed and injected in the combustion zone. All FGR duct piping should be covered with a minimum of 2" of insulation, and supported as required. The burner is designed to operate with < 30 ppm NOx corrected @ 3% O₂ throughout the firing range, when firing natural gas. See



reference: EPA/625/5-86/020, Nitrogen Oxide Control for stationary Combustion Sources. Follow burner manufacturer's recommendations for optimum operational efficiency at low NOx burner operation.

9.5.3.2 All oil burners should have two guns, one active and one spare so that one may be removed for cleaning while the other may be available for immediate use.

9.5.4 Automated shutdown: When pressure is in excess of demand sensed, the following will occur:

9.5.4.1 The damper will return to low fire position

9.5.4.2 The operating limit control opens

9.5.4.3 The main fuel valve circuit is de-energized, main fuel valve closes.

9.5.4.4 Flame is extinguished

9.5.4.5 The running lights on the control panel turn off

9.5.4.6 The blower motor continues to force air through the boiler for the post purge period.

10.0 BOILER STACK AND EMISSIONS

10.1 Boiler stack location, height, and diameter shall be determined by an engineering study conducted by a licensed professional engineer, which considers boiler/burner operational requirements, air flow around the stacks and the boiler plant and adjacent buildings, and emissions regulations. Stack gases shall not affect fresh air intakes of building ventilating or air conditioning systems. Comply with federal, state and local emissions regulations.

10.2 Generally, individual stacks on each boiler are required. A common breeching and single stack system for all boilers may be approved if documentation is provided to support the need of the request due to specific project conditions. A request for variance shall be submitted in writing through OCAMES for review and approval.

10.3 Locate diesel engine exhaust outlets so that they do not mix with building intake air.

10.4 Stacks shall be designed to provide adequate natural draft. A stack generally shall extend at least 10 feet above the highest point on the roof.

10.5 The size of the stack shall not be smaller than that recommended by the boiler manufacturer. Wherever possible, the outlet area should be sized to provide a discharge velocity at a maximum gas flow of 2000 to 3000 feet per minute.

10.6 Vents, stacks, and chimneys shall comply with NFPA 54 and NFPA 210.

10.7 Gas mains, burner headers, gas piping, etc., shall be vented according to the criteria in NFPA 85A, Prevention of Furnace Explosions in single Burner, Boiler-Furnaces and NFPA 85B, Prevention of Furnace Explosions in a Gas Multi-Burner Boiler.

10.8 Boilers shall be equipped with outlet air dampeners regardless of whether the boiler has a dedicated stack.

11.0 CONTROLS AND INSTRUMENTATION

11.1 Controls



- 11.1.1 Multi-loop industrial safety critical process programmable digital controllers are required for all control functions except burner management where specialized digital controllers are required.
 - 11.1.2 Parallel-positioning combustion controls are required for boilers ranging from 100 through 900 boiler Horsepower. For smaller fire tube boilers a single-point positioning control is more practical.
 - 11.1.3 Controls added to existing systems shall be the same manufacture and type as existing.
 - 11.2 Safety devices
 - 11.2.1 Steam Boilers shall be equipped with safety devices as defined in the most current edition of the VA boiler plant safety device manual. Electric steam boilers will comply with all element of the manual minus the fire side requirements; however it shall be equipped with electrical safety devices as defined by the manufacture. In addition to the requirements of the manufacturer an automatic shunt trip and two remote emergency stop button (one in the area of the unit and one at a centrally monitored location) shall be provided on the electrical power supply.
 - 11.2.2 Emergency fuel cut-off switches (panic buttons) shall be located at each point of egress from the plant and in the control room. The switches shall close the Natural Gas shutoff valve to the plant and de-energize all fuel oil pumps.
 - 11.3 Automatic/Remote Starting(light off)
 - 11.3.1 There shall be no automatic/remote restart of boilers after the occurrence of a fault. Faults shall activate a latching switch which must be manually reset at the boiler.
 - 11.3.2 There shall be no lead lag systems with automated/remote cycling of boiler.
 - 11.3.3 Seasonal systems must have on/off/auto switches local to the boiler. Control system shall lock out and alarm boilers that are in auto and have not fired in one month. The interlock shall be reset locally to ensure the operator is present when the boiler is fired for the first time after an outage.
 - 11.3.4 In addition to digital controls, the boilers shall come with an analog local loop control system for manual operation when the digital system is down.
 - 11.3.5 All controls shall meet the requirements of ANSI Standard Z21.13 and NFC 85 – Boiler and Combustion Systems Hazard Code – paragraph six for Automatically Fired Boilers. The controls include ignition safeguard, high temperature limit, operating temperature control, gas pressure regulator, redundant electric gas valve, water flow sensing, and a manual shut off valve.
 - 11.3.6 In addition to the requirements of the manufacturer, an automatic shunt trip and two remote emergency stop buttons (one in the area of the unit and one at a centrally monitored location on the same campus) shall be provided on the electrical supply.
 - 11.4 Monitoring and data management:
 - 11.4.1 BACNet or LONWORKS protocol Direct Digital Controls (DDC) shall be used for connection to the Building Automation System.
 - 11.4.2 Centralized Boilers and system data shall be monitored by the building automation system for data collection and logging.
 - 11.4.3 Distributed boilers shall be monitored through a building control system at a centrally monitored location. Control system shall be supervised and monitor alarm and log status, faults and safety equipment/devices. Data shall be logged for review of
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performance and faults.

- 11.4.4 Shall be by means of a Supervisory Control and Data Acquisition (SCADA) program on a computer work station reserved for only boiler system monitoring. There shall also be annunciation of alarms, pressure switches, and other operating displays on instrument panels within easy view of the attendant/operator. Controls added to existing systems shall be the same manufacture and type as existing.
- 11.5 Low-Water Cutoffs: Low water cutoffs, recycle and non-recycle, shall be provided to shut off the boiler in case of low water level in a boiler. The switches shall alarm locally and at the operator station with an audio/visual indication. The reset for the recycle switch must be local to the boiler to ensure the operator verifies the cause of the situation and investigates the impact prior to resetting. The non-recycle switch shall require a boiler restart.

12.0 OPERATION OF BOILERS

12.1 Operational Requirements

- 12.1.1 Designer shall ensure that all of the operational requirements defined below can be accommodated with the equipment and systems provided. In some cases additional connections or specific equipment for testing, and calibration may be required and must be specified and designed into the system (sample taps, test equipment, etc.).

12.2 Inspections

- 12.2.1 A testing and commissioning plan shall be developed and approved prior to the start of construction to ensure all elements are in place to accommodate successful completion. All systems shall be designed to allow for field calibration, inspection, and testing upon completion of the boiler installation. The appropriate documentation shall be provided for the purpose of receiving an operating certificate.
- 12.2.2 Boilers and safety devices shall be designed and installed to accommodate testing as defined in the VHA boiler safety device test manual and in accordance with the laws of the local jurisdiction.

12.3 Cleaning

- 12.3.1 Boilers: New and repaired boilers will contain internal surfaces that have been coated with oil. This must be removed prior to operation to avoid corrosion. A boil out chemical compound shall be used. This process requires prior planning and coordination therefore the manufacturer shall be consulted to develop a written plan and schedule for the process.
- 12.3.2 Chemical cleaning shall be used to remove any hard scale from interior surfaces. The manufacturer shall be consulted and the process approved by VACO prior to executing work. Any sort of deposit will reduce the effectiveness of the heat transfer process.
- 12.3.3 All steam, condensate, and oil piping within the plant shall be flushed and cleaned to remove all dirt, debris, oil, and scale. The flushing shall be accomplished at a minimum of 3 fps and the cleaning shall address the removal of mill scale and other contaminants in the pipe. A detergent flush shall be used to remove oils used in packaging of the piping.



13.0 FREEZE PROTECTION

- 13.1 Heat Tracing systems are not recommended for systems inside the building. It is not visually apparent that a heat cable has failed.
- 13.2 When terminal devices are in contact with freezing ambient air, steam is the preferred choice for the heat source.
- 13.3 The condensate created when steam is used for freeze protection may be returned to the boiler.

14.0 WARRANTY

- 14.1 Boilers shall be selected for the maximum warranty period offered.
 - 14.1.1 In general, the heaviest boilers, by weight, are usually the longest lived.
 - 14.1.2 Flex (bent) tube boilers offer protection against thermal shock caused by a rapid increase in thermal stresses and often have the best warranties.

15.0 MODIFICATIONS TO EXISTING PLAN

- 15.1 In addition to the equipment required for operation, the design shall provide a standby boiler and standby pumps during all phases of construction.
- 15.2 Temporary boilers and other equipment may be employed if cost effective.

16.0 CODES & STANDARDS

ASME section IV Heating Boilers

ASME B31.1 – Code for Pressure Piping

ASME B31.9 – Code for Pressure Piping, (Plants which do not generate steam over 15psig)

National Fire Protection Association

NFPA 31 – Standard for the Installation of Oil Burning Equipment

NFPA 70 – National Electrical Code

NFPA 70E – Standard for Electrical Safety in the work place

NFPA-85 – Boiler and Combustion Systems Hazard Code

NFPA 110 – Standard for Emergency and Standby Power Systems

VHA Directive 1028 – Electrical Power Distribution System

Comply with all federal, state and local codes, laws and regulations whichever is more stringent. Comply with federal executive orders and all nationally recognized industry standards (NFPA, ASHRAE, etc.).

17.0 REFERENCES

- 17.1 Design Manuals (PG-18-10); HVAC Design Manual for New, Replacement, Addition and Renovation of Existing VA Facilities: Department of Veterans Affairs, Office of Construction and Facilities Management.
- 17.2 Unified Facilities Criteria (UFC) Central Heating Plants UFC 3-430-08N
- 17.3 GSA P100 Facility Standards for Public Buildings Service
- 17.4 EPA/625/5-86/020, Nitrogen Oxide Control for Stationary Combustion Sources.



- 17.5 Heating Boiler Operators Manual, Mohammad A. Malek, 2007 McGraw-Hill
- 17.6 Cleaver Brooks – Boiler Room Guide
- 17.7 Code Requirements – International Mechanical Code latest edition
- 17.8 The VA Safety Device Testing Manual
- 17.9 VA Directive - Boiler and Boiler Plant Operations
- 17.10 VHA Directive 1028, Electrical Power Distribution System
- 17.11 VHA standard details on the TIL.
- 17.12 VA CFM Physical Security Design Manual (PSDM), latest edition
- 17.13 29 CFR 1910