

	IGER SCHEDULE	XCHAN	HEAT E	DOWN	BLOW	IUOUS	ONTIN	С
DESI	BASIS OF DESIGN	MINIMUM MAKE-UP FLOWRATE (GPM)	MINIMUM BLOWDOWN FLOWRATE (GPM)	BLOWDOWN (%)	FLASH PRESSURE (PSIG)	PLANT PRESSURE (PSIG)	PLANT LOAD (LBS/HR)	DESIG
EC-1	PENN SEPARATOR , AHRB-6-30	26	4	3	5	100	60,000	CBHX-1

DESIG	DESIGN PRESSURE (PSI)
EC-1	450
EC-2	450
EC-3	450

NOTES:

INCH DIAMETER (1"), AL-6XN STAINLESS STEEL TUBES WITH CARBON STEEL FINS.

TYPE

HORIZONTAL VENTED

DESIG	TANK HEIGHT (INCHES)	INLET (INCHES)	VENT (INCHES)	DRAIN (INCHES)	COOLING WATER TEMP (°F)	BASIS OF DESIGN	DESI
BDS-1	34	2	5	5	70	PENN SEPARATOR , A34	CST-

NOTE: PROVIDE FLANGED VENT AND DRAIN CONNECTIONS

			CAPACITY				DESIGN		MIN		SKID MOUNTED		TOTAL	APPROXIMATE	
DESIG	SERVICE	TYPE	POUNDS PER HOUR (PPH)	HORSEPOWER (HP)	MBTU's PER HOUR	EXHAUST GAS TEMPERATURE (GAS/OIL)(°F)	DESIGN PRESSURE (PSIG)	OPERATING PRESSURE (PSIG)	HEATING SURFACE (SQ.FT.)	MIN BOILER EFFICIENCY (GAS/OIL)(%)	AIR COMPRESSOR (HP)	ELECTRICAL	OPERATING WEIGHT (LBS)	OVERALL DIMENSIONS (LxWxH)	BASIS OF DESIGN
B-1	STEAM	4 PASS WET-BACK	20,700	600	20,085	375 / 383	200	100	3000	83 / 86	7½	480 / 3 / 60	65,000	24' x 10.5' x 12'	CLEAVER BROOKS, MODEL 4WI
B-2	STEAM	4 PASS WET-BACK	20,700	600	20,085	375 / 383	200	100	3000	83 / 86	7½	480 / 3 / 60	65,000	24' x 10.5' x 12'	CLEAVER BROOKS, MODEL 4WI
B-3	STEAM	4 PASS WET-BACK	20,700	600	20,085	375 / 383	200	100	3000	83 / 86	7½	480 / 3 / 60	65,000	24' x 10.5' x 12'	CLEAVER BROOKS, MODEL 4WI

NOTES: 1. SAFETY VALVE SETTINGS: 135 PSIG, 140 PSIG 2. FIRST HIGH PRESSURE CUT-OUT SETTING: 120 PSIG

SECOND HIGH PRESSURE CUT-OUT SETTING: 130 PSIG

3. MINIMUM STEAM QUALITY: 99.0% 4. ALTITUDE: 100 FEET ABOVE SEA LEVEL

5. REFER TO LOW NOX BURNER SCHEDULE FOR ADDITIONAL INFORMATION. 6. STEAM NOZZLE SHALL BE CONSTRUCTED WITH A REINFORCEMENT PAD.

				NATURAL GA	S					FORCE	ED DRAFT F	AN					
BOILER No	COMBUSTION AIR TEMPERATURE (°F)	HUIMIDITY (%)	EXCESS AIR (%) (GAS/OIL)	TURNDOWN	TRAIN INLET PRESSURE (PSIG)	NOx (PPM)	CO (PPM)	TURNDOWN	TRAIN INLET PRESSURE (PSIG)	NOx (PPM)	CO (PPM)	HP	RPM	ELECTRICAL	DUTY	VFD	BASIS OF DESIGN
1	80	50	15 / 15	10:1	10	30	50	8:1	120	90	50	40	3,500	480 / 3 / 60	INVERTER	YES	PROVIDED BY BOILER MANUFACTURER
2	80	50	15 / 15	10:1	10	30	50	8:1	120	90	50	40	3,500	480 / 3 / 60	INVERTER	YES	PROVIDED BY BOILER MANUFACTURER
3	80	50	15 / 15	10:1	10	30	50	8:1	120	90	50	40	3,500	480 / 3 / 60	INVERTER	YES	PROVIDED BY BOILER MANUFACTURER

NOTES: 1. NO COMBUSTION AIR PRE-HEAT.

3. FORCED DRAFT FAN INLET SHALL BE SCREENED.

2. GAS SPUDS SHALL BE STAINLESS STEEL.

4. EMISSIONS PARTS PER MILLION (PPM) ARE BASED ON 3% OXYGEN (O 2).

DEAERATOR SCHEDULE

DESIG TYPE	NORMAL CAPACITY (TOTAL MASS FLOW) (PPH)	MAX O2 CONTENT (CC/LITER)	MIN TURNDOWN CAPACITY	DESIGN MAKE-UP WATER TEMP (°F)	DESIGN MAKE-UP WATER FLOW (%)	DESIGN OPERATING PRESSURE (PSIG)	DESIGN OPERATING TEMPERATURE (°F)	MAX OPERATING PRESSURE (PSIG)	MIN OPERATING PRESSURE (PSIG)	STORAGE TANK MIN RETENTION AT FULL LOAD (MINUTES)	MIN RETENTION AT FULL LOAD (GAL)	APPROX. DIMENSIONS (DIA x LENGTH)	TOTAL APPROXIMATE EMPTY WEIGHT (LBS)	TOTAL APPROXIMATE FLOODED WEIGHT (LBS)	BASIS OF DESIGN
DA-1 TRAY	60,000	0.005	20:1	70	100	5	400	30	FULL VACUUM	20	2,400	6' x 15'	31,100	53,000	BFS INDUSTRIES

1. DEAERATOR SHALL BE DESIGNED AND CONSTRUCTED IN ACCORDANCE WITH ASME PRESSURE VESSEL CODES WITH 1/8" CORROSION ALLOWANCE. 2. CONSTRUCT PER HEAT EXCHANGER INSTITUTE (HEI) STANDARDS OF CONSTRUCTION. 3. STEAM NOZZLE SHALL BE CONSTRUCTED WITH A REINFORCEMENT PAD. 4. DEAERATOR MANUFACTURER SHALL PROVIDE ACCESS PLATFORM AND LADDER TO DEAERATOR HEAD FOR TRAY REMOVAL.

2 - Addendum #3 1 - Addendum #2	09/08/17	Gainesville, Tel 352.376
		Affiliated En Tioga Town 12921 SW [/]
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		CONSU

LTANTS:

Affiliated Engineers SE, Inc. Center V 1st Road Ste 205 le, Florida 32669 76.5500 Fax 352.375.3479

FORM	08-	-623

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A	three inches =
B	2 one and one half inches = one foot
C	one inch = one foot 6° 0
	three guarters inch = one foot 6, 0 2 2
D	one half inch = one foot 0 4
E	three eighths inch = one foot 0 4
F	one quarter inch = one foot 0 4 8 0 4
	one eighth inch = one foot 0 4 8 16 0 4 BHHHHHHHHHHH

NOTES:

	ECONOMIZER SCHEDULE																	
DESIGN APPROXIMATE WATER SIDE FLUE GAS SIDE																		
DESIGN TEMPERATURE (°F)	WATER FLOW CONFIGURATION	GAS FLOW CONFIGURATION	UNIT DUTY (MBTU-HR)	UNIT WET WEIGHT (LBS)	OVERALL DIMENSIONS (WxLxH)	FLUID	FLOW (PPH)	ENTERING TEMP (°F)	LEAVING TEMP (°F)	MAX PRESS DROP (PSI)	FOULING FACTOR	FLUID	FLOW (SCFM)	ENTERING TEMP (°F)	LEAVING TEMP (°F)	MAX PRESS DROP (IN. W.C.)	FOULING FACTOR	BASIS OF DESIGN
600	COUNTER FLOW	VERTICAL	450	3,067	58"x70"x95"	FEEDWATER	20,700	227	250	1.0	0.0005	FLUE GAS	4,740	369	289	0.16	0.001	CLEAVER BROOKS, CRE-42
600	COUNTER FLOW	VERTICAL	450	3,067	58"x70"x95"	FEEDWATER	20,700	227	250	1.0	0.0005	FLUE GAS	4,740	369	289	0.16	0.001	CLEAVER BROOKS, CRE-42
600	COUNTER FLOW	VERTICAL	450	3,067	58"x70"x95"	FEEDWATER	20,700	227	250	1.0	0.0005	FLUE GAS	4,740	369	289	0.16	0.001	CLEAVER BROOKS, CRE-42

1. ECONOMIZER CASING SHALL BE CONSTRUCTED OF STAINLESS STEEL. 2. ECONOMIZER INTERNALS SHALL BE CONSTRUCTED OF REMOVABLE ONE 3. ECONOMIZER SHALL MEET ALL A.S.M.E. CODE REQUIREMENTS. 4. ECONOMIZER MANUFACTURER SHALL PROVIDE SAFETY RELIEF VALVE.

SYSTEM CONNECTIONS SHALL BE A MINIMUM OF CLASS 300 CARBON STEEL.

CONDENSATE SURGE TANK SCHEDULE											
DESIGN OPERATING PRESSURE (PSIG)	MIN RETENTION AT FULL LOAD (MINUTES)	MIN RETENTION AT FULL LOAD (GAL)	TANK DIMENSIONS (DIA x OAL)	TANK EMPTY WEIGHT (LBS)	TOTAL APPROXIMATE FLOODED WEIGHT (LBS)	BASIS OF DESIGN					
		0.400		10 500							
VENTED	20	2,400	6' x 14'	12,500	34,500	BES INDUSTRIES					

SCOTCH MARINE FIRETURE BOILER SCHEDULE

LOW NOX BURNER SCHEDULE

00 F	FLANGED		
	DESIG	SYSTEM	NORMAL OPERATING MODE

NOTE: TRIPLEX SEQUENTIAL: ONE TANK OPERATIONAL, ONE TANK REGENERATION, ONE TANK STAND-BY.

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DESIC			TYDE	PUMP ROTATION	FLOW	FLOW HEAD	SUCTION /			MOTOR			MINIMUM PUMP	APPROXIMATE	
DESIG	LOCATION	SERVICE		(VERIFY)	(GPM)	(FEET H ₂ 0)	DISCHARGE	HP	RPM	ELECTRICAL	DUTY	VFD	EFFICIENCY (%)	(LBS)	DASIS OF DESIGN
CTP-1	CONDENSATE SURGE TANK	CONDENSATE TRANSFER	VERTICAL MULTISTAGE	COUNTER CLOCKWISE	84	135	2½" x 2½"	7.50	3,500	480 / 3 / 60	CONTINUOUS	NO	70.6	230	AURORA PUMPS, PVM SERIES
CTP-2	CONDENSATE SURGE TANK	CONDENSATE TRANSFER	VERTICAL MULTISTAGE	COUNTER CLOCKWISE	84	135	2½" x 2½"	7.50	3,500	480 / 3 / 60	CONTINUOUS	NO	70.6	230	AURORA PUMPS, PVM SERIES
CTP-3	CONDENSATE SURGE TANK	CONDENSATE TRANSFER	VERTICAL MULTISTAGE	COUNTER CLOCKWISE	42	135	2" x 2"	3.00	3,500	480 / 3 / 60	CONTINUOUS	NO	64.8	131	AURORA PUMPS, PVM SERIES
BFP-1	DEAERATOR	BOILER FEED WATER	VERTICAL MULTISTAGE	COUNTER CLOCKWISE	46	370	2" x 2"	7.50	3,500	480 / 3 / 60	INVERTER	YES	66.1	197	AURORA PUMPS, PVM SERIES
BFP-2	DEAERATOR	BOILER FEED WATER	VERTICAL MULTISTAGE	COUNTER CLOCKWISE	46	370	2" x 2"	7.50	3,500	480 / 3 / 60	INVERTER	YES	66.1	197	AURORA PUMPS, PVM SERIES
BFP-3	DEAERATOR	BOILER FEED WATER	VERTICAL MULTISTAGE	COUNTER CLOCKWISE	46	370	2" x 2"	7.50	3,500	480 / 3 / 60	INVERTER	YES	66.1	197	AURORA PUMPS, PVM SERIES
FOP-1	FUEL OIL PUMP PIT	No 2 FUEL OIL	ROTARY POSITIVE DISPLACEMENT	COUNTER CLOCKWISE	11	290	1¼" x 1¼"	2.00	1,725	480 / 3 / 60	CONTINUOUS	NO	-	120	PREFERRED, LO-204
FOP-2	FUEL OIL PUMP PIT	No 2 FUEL OIL	ROTARY POSITIVE DISPLACEMENT	COUNTER CLOCKWISE	11	290	1¼" x 1¼"	2.00	1,725	480 / 3 / 60	CONTINUOUS	NO	-	120	PHILLIPS FUEL SYSTEMS, D-15

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DEAERATOR CONNECT	IONS S	SCHEDULE					ST	EAN	I TRAP	SCHEDL	JLE					
<u>DESCRIPTION</u>	<u>MINIMUM</u> NNECTION SI2 (DIA)	ZE QUANTITY EACH			DESC		TYPE	TRAP	MINIMUM INLET	MINIMUM DIFF PRESS		FLOW RAT (LB/HR)	Ē	STEAM (°	1 TEMP F)	
PUMPED CONDENSATE INLET : STEAM INLET :	3" 8"	1			DESG	GENERAL LOCATION	TIFE	SIZE	(PSIG)	(F313)	OPER FLOW	SAFETY FACTOR	DESIGN FLOW	OPER	MAX	BASIS OF DESIGN
RELIEF VALVE OUTLET :	1½"	1		$\left\{ \right\}$	T-01	100S STEAM HEADER END DRIP	INVERTED BUCKET	1/2"	100	80	110	3	330	338	361	-
TEMPERATURE INDICATOR / TRANSMITTER :	3 ₄ "	3		$\left\langle \right\rangle$	T-02	100S STEAM HEADER END DRIP	INVERTED BUCKET	1/2"	100	80	110	3	330	338	361	-
PRESSURE INDICATOR :	3 ₄ "	1		\mathbf{i}	T-03	100S WHISTLE VALVE DRIP	INVERTED BUCKET	1/2"	100	80	5	3	15	338	361	-
ATMOSPHERIC VENT :	1½"	1		>	T-04	DEAERATOR PRV	INVERTED BUCKET	1/2"	100	80	110	3	330	338	361	-
HEATER MANWAY :	18"	1			T-05	5S AT REDUCING STATION	FLOAT & THERMOSTATIC	34"	5	1/4	16	2.5	40	227	250	-
HIGH PRESSURE RETURN :	2"	1		Z	T-06	100S MAIN TO DISTRIBUTION	INVERTED BUCKET	¹ /2"	100	80	64	3	191	338	361	-
VACUUM BREAKER :	2½"	1			T-07	100S MAIN TO REDUCING STATION	INVERTED BUCKET	1/2"	100	80	12	3	36	338	361	-
	-			\$	T-08	100S AT REDUCING STATION	INVERTED BUCKET	1/2"	100	80	12	3	36	338	361	-
BOILER FEED WATER PUMP RECIRCULATION :	1%"	1			T-09	15S AT REDUCING STATION	FLOAT & THERMOSTATIC	1/2"	15	1/4	16	2.5	40	250	262	-
	2			2	T-10	5S MAIN TO DA-1	FLOAT & THERMOSTATIC	1"	5	1/4	16	2.5	40	227	250	-
BOILER FEED WATER PUMP SUCTION :	6"	1		\sim	T-11	5S MAIN FROM CBHX-1	FLOAT & THERMOSTATIC	3 ₄ "	5	1/4	16	2.5	40	227	250	-
OXYGEN SAMPLE POINT :	3 ₄ "	1		$\left\langle \right\rangle$	T-12	15S END OF MAIN DRIP	INVERTED BUCKET	¹ /2"	15	12	20	3	60	250	262	-
STORAGE MANWAY :	- 12"x16"	2		>	T-13	15S MAIN TO HEATING EQUIPMENT	INVERTED BUCKET	¹ /2"	15	12	20	3	60	250	262	-
OVERFLOW :	4"	1			T-14	HV-B-1 EQUIPMENT DRIP	FLOAT & THERMOSTATIC	1½"	5	1/4	383	2.5	950	227	262	-
LEVEL CONTROL :	1%"	2		5	T-15	HV-B-2 EQUIPMENT DRIP	FLOAT & THERMOSTATIC	1½"	5	1/4	383	2.5	950	227	262	-
GAUGE GLASS :	1%"	2			T-16	HV-B-3 EQUIPMENT DRIP	FLOAT & THERMOSTATIC	1 ¹ / ₂ "	5	1/4	383	2.5	950	227	262	-
CHEMICAL FEED :	1%"	1		2	T-17	100S EMERGENCY BOILER	INVERTED BUCKET	¹ /2"	100	80	33	3	100	338	361	-
MANUAL DRAIN :	1½"	1														
	• 2			\mathbf{x}												
			<u>ل</u> ،	<u>/2</u>												
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STEAM VENT SILENC	ER SCI	HEDULE			4				λ		\sim	\mathcal{A}	^	\land		
DESIG LOCATION FLOW OUT (PPH) OUT (INC	LET ZE E CH)	BASIS OF DESIGN														

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DEAERATOR CONNEC	TION	S SCHEDULE				ST	EAN	/I TRAP	SCHEDI	JLE					$\sum_{i=1}^{n}$
DESCRIPTION	<u>MINIMU</u> CONNECTIO (DIA)	<u>JM</u> DN SIZE QUANTITY EACH		DESC		TYPE	TRAP	MINIMUM	MINIMUM DIFF PRESS		FLOW RAT (LB/HR)	Ē	STEAM (°F	TEMP	
PUMPED CONDENSATE INLET :	3" 8"	1		DESG	GENERAL LOCATION	ITE	SIZE	(PSIG)	(PSIG)	OPER FLOW	SAFETY FACTOR	DESIGN FLOW	OPER	MAX	BASIS OF DESIGN
RELIEF VALVE OUTLET :	1½"	1		T_01	100S STEAM HEADER END DRIP		1, "	100	80	110	3	330	338	361	_
MPERATURE INDICATOR / TRANSMITTER :	3,"	3	2	T-02			/2 1/_"	100	80	110	3	330	338	361	
ESSURE INDICATOR :	'4 3,"	1		T-02			/2 1/_"	100	80	5	3	15	338	361	
IOSPHERIC VENT :	"4 1 %"	1	<u> </u>	T-04	DEAFRATOR PRV	INVERTED BUCKET	1/2 1/2"	100	80	110	3	330	338	361	-
TER MANWAY :	18"	1		T-05	5S AT REDUCING STATION	FLOAT & THERMOSTATIC	2 3,"	5	1/4	16	2.5	40	227	250	-
H PRESSURE RETURN :	2"	1	~	T-06	100S MAIN TO DISTRIBUTION	INVERTED BUCKET	⁷ 4 1/2"	100	80	64	3	191	338	361	-
UUM BREAKER :	21/"	1	\sim	T-07	100S MAIN TO REDUCING STATION	INVERTED BUCKET	1/2"	100	80	12	3	36	338	361	-
	2'2			T-08	100S AT REDUCING STATION	INVERTED BUCKET	1/2"	100	80	12	3	36	338	361	-
ER FEED WATER PUMP RECIRCULATION	J: 11/-"	1		T-09	15S AT REDUCING STATION	FLOAT & THERMOSTATIC	1/2"	15	1/4	16	2.5	40	250	262	-
	1/2		\mathbf{i}	T-10	5S MAIN TO DA-1	FLOAT & THERMOSTATIC	1"	5	1/4	16	2.5	40	227	250	-
R FEED WATER PUMP SUCTION :	6"	1	\geq	T-11	5S MAIN FROM CBHX-1	FLOAT & THERMOSTATIC	34"	5	1/4	16	2.5	40	227	250	-
EN SAMPLE POINT :	3."	1	\langle	T-12	15S END OF MAIN DRIP	INVERTED BUCKET	1/2"	15	12	20	3	60	250	262	-
AGE MANWAY :	74 12"x16	5" 2	5	T-13	15S MAIN TO HEATING EQUIPMENT	INVERTED BUCKET	1/2"	15	12	20	3	60	250	262	-
FLOW :	4"	1		T-14	HV-B-1 EQUIPMENT DRIP	FLOAT & THERMOSTATIC	1½"	5	1/4	383	2.5	950	227	262	-
	11/ "	2		T-15	HV-B-2 EQUIPMENT DRIP	FLOAT & THERMOSTATIC	1½"	5	1/4	383	2.5	950	227	262	-
GE GLASS ·	1 ⁷ 2 11/"	2	(T-16	HV-B-3 EQUIPMENT DRIP	FLOAT & THERMOSTATIC	1½"	5	1/4	383	2.5	950	227	262	-
	1 ⁷ 2	1	>	T-17	100S EMERGENCY BOILER	INVERTED BUCKET	¹ / ₂ "	100	80	33	3	100	338	361	-
	1 ⁷ 4 1 1 ''	1	$\left(\right)$												
	1 <i>°</i> 2														
			2												
STEAM VENT SILEN	CER S	SCHEDULE		4	1			λ	λ	λ	λ			\sim	
	UTLET														
/S-1 100 STEAM HEADER 21.000	16 VA	ANEC MODEL 521-16													

NOTES:

12 dB MINIMUM AT 63 Hz
17 dB MINIMUM AT 125-250 hZ
25 dB MINIMUM AT 250-500 Hz
34 dB MINIMUM AT 500-8000 Hz

ENGINEER-OF-RECORD JACK STEWART NEALE	FL. P.E. NO. 42678	ARCHITECT/ENGINEERS:

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	AKEA Project No. 083-14

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GENERAL NOTES:

MAINTENANCE, AND CALIBRATION, SHALL BE EASILY AND SAFELY ACCESSIBLE BY PERSONS STANDING AT FLOOR LEVEL, OR STANDING ON PERMANENT PLATFORMS, WITHOUT THE USE OF PORTABLE LADDERS. EXAMPLES OF THESE ITEMS INCLUDE, BUT ARE NOT LIMITED TO: ALL TYPES OF VALVES, FILTERS AND STRAINERS, TRANSMITTERS, CONTROL DEVICES. PRIOR TO COMMENCING INSTALLATION WORK, REFER CONFLICTS BETWEEN THIS REQUIREMENT AND CONTRACT DRAWINGS TO THE RESIDENT ENGINEER FOR RESOLUTION.

								WAIER	SOFI	ENER SCI	HEDULE								
			WATER	WATER			GRAIN	NORMAL	ΡΕΔΚ	MAXIMUM		VESSEI	ΜΑΧΙΜΙΙΜ	MAXIMUM	BRINE TAI	NK			
DESIG	SYSTEM	NORMAL OPERATING MODE	HARDNESS INLET (PPM)	HARDNESS OUTLET (PPM)	OPERATING OPE TEMPERATURE PRE (°F)	ERATING ESSURE (PSI)	CAPACITY PER TANK (GRAINS)	FLOW RATE (GPM)	FLOW RATE (GPM)	DROP AT NORMAL FLOW RATE (PSI)	VESSEL SIZE (EACH TANK) (DIA x H)	PRESSURE RATING (PSI)	REGENERATION TIME (MINUTES)	BACKWASH FLOW (GPM)	CAPACITY (GAL)	DIMENSIONS (DIA x H)	ELECTRICAL	APPROX WEIGHT (LBS)	BASIS OF DESIGN
WSF-1	BOILER MAKE-UP (NP)	TRIPLEX SEQUENTIAL	120	0	70	65	900,000	65	210	15	42" x 60"	100	120	15	500	57" x 63"	120 / 1 / 60	10,000	WATER KING, MF-240S-2

PUMP SCHEDULE

		APPR	COVED	FOR
Drawing Title MECHANICAL SCHEDULES	Project Title REPLACE BOILE AT THE MALCON	RS - FCA D 1 RANDALL	, energy . Vamc	Project Numb 573-14- Building Num
Approved: Project Director	Location GAINESVILLE, I Date JULY 8, 2016	FLORIDA Checked JSN	Drawn RWD	Drawing Num

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1. ALL ITEMS THAT REQUIRE ACCESS, SUCH AS FOR OPERATING, CLEANING, SERVICING,

