CONTINUOUS BLOWDOWN HEAT EXCHANGER SCHEDULE **ECONOMIZER SCHEDULE** 1. ALL ITEMS THAT REQUIRE ACCESS, SUCH AS FOR OPERATING, CLEANING, SERVICING, MAINTENANCE, AND CALIBRATION, SHALL BE EASILY AND SAFELY ACCESSIBLE BY PERSONS **APPROXIMATE** LOAD PRESSURE PRESSURE BLOWDOWN BLOWDOWN MAKE-UP DESIGN DESIGN STANDING AT FLOOR LEVEL, OR STANDING ON PERMANENT PLATFORMS, WITHOUT THE USE OF GAS FLOW UNIT DUTY WATER FLOW ENTERING LEAVING MAX PRESS ENTERING BASIS OF DESIGN DESIG PRESSURE TEMPERATURE WEIGHT BASIS OF DESIGN FOULING PORTABLE LADDERS. EXAMPLES OF THESE ITEMS INCLUDE, BUT ARE NOT LIMITED TO: ALL CONFIGURATION | CONFIGURATION | (MBTU-HR) (%) | FLOWRATE | FLOWRATE DIMENSIONS TEMP TEMP DROP TEMP TEMP (LBS) (LBS/HR) (PSIG) (PSIG) (PSI) TYPES OF VALVES, FILTERS AND STRAINERS, TRANSMITTERS, CONTROL DEVICES. PRIOR TO (SCFM) **FACTOR** (GPM) (WxLxH) (PSI) (°F) (IN. W.C.) COMMENCING INSTALLATION WORK, REFER CONFLICTS BETWEEN THIS REQUIREMENT AND CONTRACT DRAWINGS TO THE RESIDENT ENGINEER FOR RESOLUTION. EC-1 COUNTER FLOW PENN SEPARATOR . AHRB-6-30 VERTICAL FEEDWATER 0.001 CLEAVER BROOKS, CRE-42 EC-2 0.001 CLEAVER BROOKS, CRE-42 450 COUNTER FLOW VERTICAL EC-3 COUNTER FLOW VERTICAL 1.0 0.001 CLEAVER BROOKS, CRE-42 3. ECONOMIZER SHALL MEET ALL A.S.M.E. CODE REQUIREMENTS. 1. ECONOMIZER CASING SHALL BE CONSTRUCTED OF STAINLESS STEEL 2. ECONOMIZER INTERNALS SHALL BE CONSTRUCTED OF REMOVABLE ONE 4. ECONOMIZER MANUFACTURER SHALL PROVIDE SAFETY RELIEF VALVE. INCH DIAMETER (1"), AL-6XN STAINLESS STEEL TUBES WITH CARBON 5. SYSTEM CONNECTIONS SHALL BE A MINIMUM OF CLASS 300 FLANGED STEEL FINS. CARBON STEEL. CONDENSATE SURGE TANK SCHEDULE WATER SOFTENER SCHEDULE **BLOWDOWN SEPARATOR SCHEDULE** DESIGN PRESSURE VESSEL MAXIMUM HARDNESS HARDNESS TEMPERATURE PRESSURE PER TANK OPERATING OPERATING CAPACITY CONTINUOUS APPROXIMATE VESSEL SIZE VESSEL SIZE (EACH TANK) PRESSURE REGENERATION BACKWASH RATING TIME FLOW INLET VENT FLOW DROP AT OPERATING | RETENTION AT RETENTION AT **EMPTY** FLOW CAPACITY DIMENSIONS ELECTRICAL WEIGHT HEIGHT BASIS OF DESIGN DESIG FLOODED OPERATING (INCHES) (INCHES) (INCHES) DIMENSIONS BASIS OF DESIGN SYSTEM FLOW RATE BASIS OF DESIGN TEMP PRESSURE FULL LOAD WEIGHT RATE CONTINUOUS FULL LOAD WEIGHT (DIA x OAL) (PSI) (GPM) (DIA x H) (GPM) | (GAL) | (DIA x H) (MINUTES) FLOW RATE (PSI) (MINUTES) (LBS) 218 120 / 1 / 60 | 10,000 | MARLO MR-900-2 70 PENN SEPARATOR, A34 CST-1 HORIZONTAL VENTED 2,400 6' x 14' 12,500 BFS INDUSTRIES WSF-1 | BOILER MAKE-UP (NP) | TRIPLEX SEQUENTIAL | 900,000 150 100 500 57" x 63" 2 | 5 | 5 | 34,500 120 65 NOTE: TRIPLEX SEQUENTIAL: ONE TANK OPERATIONAL, ONE TANK REGENERATION, ONE TANK STAND-BY. NOTE: PROVIDE FLANGED VENT AND DRAIN CONNECTIONS SCOTCH MARINE FIRETUBE BOILER SCHEDULE PUMP SCHEDULE **APPROXIMATE** MINIMUM SKID MOUNTED APPROXIMATE EXHAUST GAS DESIGN OPERATING MIN BOILER HEATING OVERALL PUMP ROTATION FLOW HEAD PUMP POUNDS OPERATING TYPE DESIG LOCATION SERVICE BASIS OF DESIGN SERVICE HORSEPOWER | MBTU's TEMPERATURE | PRESSURE PRESSURE EFFICIENCY BASIS OF DESIGN WEIGHT SURFACE COMPRESSOR DIMENSIONS EFFICIENCY (VERIFY) (GPM) (FEET H₂0) DISCHARGE PER HOUR WEIGHT (PSIG) (GAS/OIL)(%) (LBS) (GAS/OIL)(°F) (PSIG) PER HOUR (HP) RPM | ELECTRICAL (SQ.FT.) (LxWxH) DUTY VFD (PPH) (LBS) CTP-1 4 PASS WET-BACK 480 / 3 / 60 24' x 10.5' x 12' CLEAVER BROOKS, MODEL 4WI 65,000 CONDENSATE SURGE TANK CONDENSATE TRANSFER VERTICAL MULTISTAGE COUNTER CLOCKWISE CONTINUOUS NO 135 480 / 3 / 60 AURORA PUMPS, PVM SERIES 3000 480 / 3 / 60 STEAM 100 83 / 86 24' x 10.5' x 12' CLEAVER BROOKS, MODEL 4WI 65,000 CTP-2 230 CONDENSATE SURGE TANK CONDENSATE TRANSFER VERTICAL MULTISTAGE COUNTER CLOCKWISE 135 CONTINUOUS NO AURORA PUMPS, PVM SERIES 20,700 20,085 200 100 3000 83 / 86 65,000 24' x 10.5' x 12' CLEAVER BROOKS, MODEL 4WI STEAM 4 PASS WET-BACK 375 / 383 480 / 3 / 60 COUNTER CLOCKWISE CTP-3 CONDENSATE SURGE TANK CONDENSATE TRANSFER VERTICAL MULTISTAGE 135 CONTINUOUS NO AURORA PUMPS, PVM SERIES AURORA PUMPS, PVM SERIES BFP-1 **BOILER FEED WATER** VERTICAL MULTISTAGE **DEAERATOR** COUNTER CLOCKWISE INVERTER YES 66.1 **BOILER FEED WATER** BFP-2 COUNTER CLOCKWISE **DEAERATOR** VERTICAL MULTISTAGE 370 YES AURORA PUMPS, PVM SERIES 480 / 3 / 60 BFP-3 AURORA PUMPS, PVM SERIES **DEAERATOR** BOILER FEED WATER COUNTER CLOCKWISE INVERTER YES VERTICAL MULTISTAGE 3,500 480 / 3 / 60 . SAFETY VALVE SETTINGS: 135 PSIG, 140 PSIG 3. MINIMUM STEAM QUALITY: 99.0% 2. FIRST HIGH PRESSURE CUT-OUT SETTING: 120 PSIG 4. ALTITUDE: 100 FEET ABOVE SEA LEVEL FUEL OIL PUMP PIT No 2 FUEL OIL ROTARY POSITIVE DISPLACEMENT COUNTER CLOCKWISE CONTINUOUS | NO PREFERRED, LO-204 SECOND HIGH PRESSURE CUT-OUT SETTING: 130 PSIG 5. REFER TO LOW NOX BURNER SCHEDULE FOR ADDITIONAL INFORMATION. FOP-2 FUEL OIL PUMP PIT No 2 FUEL OIL ROTARY POSITIVE DISPLACEMENT | COUNTER CLOCKWISE 290 2.00 | 1,725 | 480 / 3 / 60 | CONTINUOUS | NO 120 PHILLIPS FUEL SYSTEMS, D-15 6. STEAM NOZZLE SHALL BE CONSTRUCTED WITH A REINFORCEMENT PAD. LOW NOx BURNER SCHEDULE STEAM TRAP SCHEDULE DEAERATOR CONNECTIONS SCHEDULE NATURAL GAS FUEL OIL No 2 FORCED DRAFT FAN COMBUSTION HUIMIDITY BOILER AIR (%) TRAIN INLET BASIS OF DESIGN CO NOx NOx TEMPERATURE (°F) (GAS/OIĹ) TURNDOWN PRESSURE TURNDOWN PRESSURE RPM ELECTRICAL DUTY FLOW RATE STEAM TEMP (PPM) (PPM) (PPM) MINIMUM (PSIG) **DESCRIPTION** INLET DIFF PRESS (LB/HR) **QUANTITY EACH** (°F) BASIS OF DESIGN GENERAL LOCATION TYPE PRESSURE (PSIG) SIZE PUMPED CONDENSATE INLET: OPER | SAFETY | DESIGN | (PSIG) 15 / 15 10:1 INVERTER YES PROVIDED BY BOILER MANUFACTURES OPER | MAX FLOW FACTOR FLOW STEAM INLET: 15 / 15 10:1 50 8:1 120 INVERTER YES PROVIDED BY BOILER MANUFACTURER 15 / 15 10:1 50 8:1 120 3,500 INVERTER YES PROVIDED BY BOILER MANUFACTURER 50 10 30 90 50 40 480 / 3 / 60 RELIEF VALVE OUTLET T-01 100S STEAM HEADER END DRIP INVERTED BUCKET 338 361 110 330 TEMPERATURE INDICATOR / TRANSMITTER T-02 100S STEAM HEADER END DRIP INVERTED BUCKET 330 338 361 PRESSURE INDICATOR 100S WHISTLE VALVE DRIP T-03 INVERTED BUCKET 338 361 100 80 15 ATMOSPHERIC VENT: T-04 DEAERATOR PRV INVERTED BUCKET 100 110 330 338 361 1. NO COMBUSTION AIR PRE-HEAT. 3. FORCED DRAFT FAN INLET SHALL BE SCREENED. GAS SPUDS SHALL BE STAINLESS STEEL. **HEATER MANWAY** T-05 4. EMISSIONS PARTS PER MILLION (PPM) ARE BASED ON 3% OXYGEN (O 2). 5S AT REDUCING STATION FLOAT & THERMOSTATIC 1/4 227 250 40 T-06 HIGH PRESSURE RETURN: 100S MAIN TO DISTRIBUTION INVERTED BUCKET 191 338 361 64 VACUUM BREAKER: T-07 100S MAIN TO REDUCING STATION INVERTED BUCKET 338 361 12 36 T-08 100S AT REDUCING STATION INVERTED BUCKET 100 12 36 338 361 DEAERATOR SCHEDULE T-09 BOILER FEED WATER PUMP RECIRCULATION: 15S AT REDUCING STATION FLOAT & THERMOSTATIC 1/4 40 250 T-10 5S MAIN TO DA-1 227 250 FLOAT & THERMOSTATIC 40 STORAGE TANK DESIGN T-11 5S MAIN FROM CBHX-1 227 250 FLOAT & THERMOSTATIC 1/4 16 40 BOILER FEED WATER PUMP SUCTION: NORMAL CAPACITY APPROXIMATE APPROXIMATE MAKE-UP OPERATING OPERATING OPERATING OPERATING MIN MAKE-UP APPROX. TURNDOWN TYPE (TOTAL MASS FLOW) CONTENT EMPTY FLOODED BASIS OF DESIGN DESIG T-12 15S END OF MAIN DRIP INVERTED BUCKET 12 250 262 RETENTION AT RETENTION AT 20 60 WATER TEMP | WATER FLOW | PRESSURE | TEMPERATURE | PRESSURE | PRESSURE OXYGEN SAMPLE POINT: DIMENSIONS WEIGHT CAPACITY WEIGHT (CC/LITER) FULL LOAD FULL LOAD (%) (PSIG) (°F) (PSIG) (PSIG) (DIA x LENGTH) (LBS) (LBS) T-13 15S MAIN TO HEATING EQUIPMENT INVERTED BUCKET 12 60 250 262 STORAGE MANWAY 12"x16" (MINUTES) T-14 FLOAT & THERMOSTATIC 227 262 HV-B-1 EQUIPMENT DRIP 383 **OVERFLOW:** DA-1 TRAY 60.000 0.005 20:1 100 400 30 FULL VACUUM 2,400 53,000 BFS INDUSTRIES 6' x 15' T-15 **HV-B-2 EQUIPMENT DRIP** FLOAT & THERMOSTATIC 227 1/4 383 950 LEVEL CONTROL T-16 **HV-B-3 EQUIPMENT DRIP** 227 262 FLOAT & THERMOSTATIC 1/4 383 950 2.5 **GAUGE GLASS:** T-17 100S EMERGENCY BOILER 100 338 361 INVERTED BUCKET 100 80 33 CHEMICAL FEED 3. STEAM NOZZLE SHALL BE CONSTRUCTED WITH A REINFORCEMENT PAD. 1. DEAERATOR SHALL BE DESIGNED AND CONSTRUCTED IN ACCORDANCE WITH ASME MANUAL DRAIN: PRESSURE VESSEL CODES WITH 1/8" CORROSION ALLOWANCE. 4. DEAERATOR MANUFACTURER SHALL PROVIDE ACCESS PLATFORM AND LADDER TO DEAERATOR HEAD FOR TRAY REMOVAL. 2. CONSTRUCT PER HEAT EXCHANGER INSTITUTE (HEI) STANDARDS OF CONSTRUCTION. STEAM VENT SILENCER SCHEDULE FLOW (PPH) SIZE (INCH) BASIS OF DESIGN DESIG LOCATION SVS-1 100 STEAM HEADER 21,000 16 VANEC MODEL 521-16 NOTES: 1. 12 dB MINIMUM AT 63 Hz 17 dB MINIMUM AT 125-250 hZ 25 dB MINIMUM AT 250-500 Hz 34 dB MINIMUM AT 500-8000 Hz FINAL DESIGN APPROVED FOR CONSTRUCTION Drawing Title Project Title ENGINEER-OF-RECORD FL. P.E. NO JACK STEWART NEALE 42678 ARCHITECT/ENGINEERS: CONSULTANTS: Office of 573-14-600 REPLACE BOILERS - FCA D, ENERGY MECHANICAL SCHEDULES AKEAINC Construction Affiliated Engineers
Affiliated Engineers SE, Inc. **Building Number** AT THE MALCOM RANDALL VAMC and Facilities 3603 NW 98th Street, Suite B Approved: Project Director **Drawing Number** Management GAINESVILLE, FLORIDA Gainesville, FL 32606 Tioga Town Center Phone: (352) 474-6124 09/14/17 - Addendum #4 12921 SW 1st Road Ste 205 MP601 Fax: (352) 553-4437 - Addendum #3 09/08/17 Gainesville, Florida 32669 Checked Tel 352.376.5500 Fax 352.375.3479 COA: FL #26693 08/30/17 **JULY 8, 2016** RWD - Addendum #2 **JSN** AKEA Project No. 083-14 Date **Revisions:** VA FORM 08-623

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